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OXIDATION OF XYLOSE – METHANOL MIXTURE INTO METHYL LACTATE AND METHYL GLYCOLATE ON CeO₂-SnO₂/Al₂O₃ CATALYST

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The development of catalytic methods for xylose transformation as renewable raw material into value-added chemicals such as lactic and glycolic acid esters has been the subject of intensive research in recent years. Thus, methyl lactate and methyl glycolate are used as a starting material for the production of lactide and glycolide – an important monomers for the production of biodegradable polymers. The aim of this work was to search of simple effective catalyst for transformation of xylose into methyl esters of lactic and glycolic acids. For this purpose, tin-containing alumina doped with CeO₂, MoO₃ and CuO oxides were synthesized by impregnation method. Textural and structural parameters of obtained MeO-SnO₂/Al₂O₃ mixed oxides were estimated from the results of low-temperature adsorption-desorption of nitrogen and X-ray diffraction. The formation of morphology ceria close to octahedra for CeO₂-SnO₂/Al₂O₃ sample is confirmed by the X-ray phase analysis data and SEM microphotographs. The UV spectroscopy data indicates the nanosize of tin dioxide particles on the γ -Al₂O₃ surface. According to the titration results, CeO₂-SnO₂/Al₂O₃ is acid mixed oxide with $H_0 \leq -3.0$. The catalytic conversion of xylose solution in methanol was carried out in rotated autoclaves and in a flow stainless steel reactor with a fixed bed of catalyst. The products of the target reaction $C_5H_{10}O_5 + 2CH_3OH + 1/2O_2 = C_4H_8O_3 + C_3H_6O_3 + 2H_2O$ were analyzed by ¹³C NMR. It was found that a complete conversion of 4 % xylose solution in a 70 % aqueous methanol solution occurs with the formation of methyl lactate (42 %) and methyl glycolate (24 %) on the developed CeO₂-SnO₂/Al₂O₃ catalyst loading of 3.5 mmol C₅H₁₀O₅/g_{cat}/h at 190 °C/3.0 MPa in air flow. The path of the reaction is proposed, namely: the ^{IV}Sn⁴⁺ ions in CeO₂-SnO₂/Al₂O₃ catalyst as Lewis acid sites promote retro-aldol xylose condensation and further Cannizzaro rearrangement of intermediate methyl pyruval hemiacetal into methyl lactate. And CeO₂ provides selective oxidation of glycol aldehyde formed as a result of aldol decondensation of xylose to methyl glycolate.

Keywords: xylose conversion, methyl lactate, methyl glycolate, mixed oxide, CeO₂, SnO₂

INTRODUCTION

Xylose can be considered as a platform chemical, which is an intermediate to a plethora of chemicals such as xylitol, lactic acid and its esters and also furfural, in turn a key building block to produce several chemicals [1]. Lactic acid methyl ester, methyl lactate (ML), is used mainly as a cellulose acetate solvent [2] and as a starting material for the production of lactic acid oligomers and lactide [3, 4]. Methyl glycolate (MG), glycolic acid methyl ester, can be used as a good solvent instead of chlorinated hydrocarbons and as precursor for obtaining glycolide – an important monomer for the production of biodegradable polyglycolide [5].

The chemical ML or MG is usually produced by the esterification of lactic or glycolic acids with methanol [6]. Retro-aldol condensation of available hexose - glucose or fructose in the presence of methanol is a promising alternative way to obtaining methyl lactate, which has been

developed recent years. In particular, we have found that SnO₂-containing oxides prepared by a simple wet impregnation of alumina provides 70 % yield of methyl lactate at 180 °C during continuous conversion of fructose in aqueous methanol solution [7]. In this article a possible scheme of fructose transformation into ethyl lactate on L-acid ^{IV}Sn⁴⁺ sites is presented. It was interesting to study similar transformation of pentose – xylose into esters of lactic and glycolic acids. In the case of xylose, retro-aldol splitting leads to C3 (glyceraldehyde) and C2 (glycol aldehyde) fragments. Further glyceraldehyde can dehydrate to methyl pyruvate that in the presence of methanol can rearrangement according to Cannizzaro into methyl lactate. But intermediate glycol aldehyde must be oxidized in the presence of methanol to methyl glycolate on appropriate catalysts. Thus, a studied reaction can be written as follows: $C_5H_{10}O_5 + 2CH_3OH + 1/2O_2 = C_4H_8O_3 + C_3H_6O_3 + 2H_2O$. For glycol aldehyde

oxidation we have doped the SnO₂/Al₂O₃ catalyst with CeO₂, MoO₃ and CuO oxides as it is recommended in [8].

In this communication the results on transformation xylose-methanol mixture into methyl esters of lactic and glycolic acids over several mixed oxides supported by alumina are presented.

EXPERIMENTAL

MeO-SnO₂/Al₂O₃ mixed oxides were obtained by impregnating of granulated γ -Al₂O₃ (AOA, Ukraine) with an aqueous solution of salts SnCl₄·5H₂O, Ce(NO₃)₃·6H₂O, Cu(NO₃)₂·6H₂O, (NH)₆Mo₇O₂₄·4H₂O with subsequent heat treatment at 550 °C for 2 h. For impregnation, a fraction of 0.5–2.0 mm of carrier granules pre-dried at 250 °C was used. After calcination, the content of tin dioxide in the samples was 10 % by mass, and the content of other metal oxides was 5 %.

Thermal studies were carried out on a serial derivative Q-1500D (Hungary) in the temperature range of 290–1270 K using a platinum crucible. The sample heating rate was 10 K min⁻¹. The textural parameters of the oxides were determined by the method of low-temperature nitrogen adsorption-desorption on a Quantachrome Nova 2200e Surface Area and Pore Size Analyzer. To analyze the morphology of the sample, a high-resolution auto-emission scanning electron microscope (SEM JSM-6700, JEOL, Japan) with energy-dispersive and cathode-luminescent attachments was used (resolution 1.0–2.2 nm). X-ray patterns of the catalysts were recorded on a DRON-4-07 diffractometer in the Cu K α line of the anode with a nickel filter in the reflected beam with the Bragg-Brentano shooting geometry. Diffuse reflectance UV-Vis spectra were recorded using a Perkin Elmer Lambda 40 spectrophotometer equipped with a diffuse reflectance camera and an integrating sphere (Labsphere RSA-PE-20). MgO was used as a standard. To determine the band gap E_0 , the reflection spectra were converted to the absorption spectra using the Kubelka–Munk formula, $F = (hv(1 - R)^2/2R)^{1/2}$. The value of E_0 was determined from the almost linear long-wavelength segment of the absorption band section, extrapolated to the intercept with the abscissa. The strength of the acid sites of the samples in terms of the Hammett H_0 function was determined according to the standard method

using the appropriate Hammett indicators (Aldrich) [9]. To determine the total concentration of acid sites, the method of reverse titration of *n*-butylamine adsorbed on the surface of the samples with a solution of hydrochloric acid in the presence of the indicator bromothymol blue [9] was used.

The catalytic conversion of a 10 % xylose solution (*h*) in a methanol was previously carried out in autoclaves with Teflon liners (25 ml) with rotation at a speed of 60 rpm for a certain time at the temperature of 160 °C, 3 h. Further, the catalytic experiment was carried out in a stainless-steel flow reactor with a diameter of 8 mm with a fixed catalyst layer (1.7 g, 3 cm³) at temperatures of 160–190 °C and the pressure of 3.0 MPa. The reaction mixture (4 % xylose solution in a 70 % aqueous methanol solution) for contact with the heated catalyst layer was fed from top to bottom using a Waters-590 pump with the same volume velocity LHSV = 4÷6 h⁻¹, which corresponded to a feed rate of 2÷3.5 mmol C₅H₁₀O₅/g_{cat}/h interval. Air was used as a carrier gas, with air oxygen serving as an oxidizer. Under these conditions, the components of the initial solution and transformation products were in a liquid state.

The xylose conversion products were identified by ¹³C NMR spectra (“Bruker Avance-400” spectrometer Karlsruhe, Germany) and by liquid chromatography (Waters HPLC system; Alliance, MA, USA). Xylose conversion (%) and product selectivity (mol %) were calculated from ¹³C NMR spectra by the corresponding ratio of the planes of the signals of methyl lactate at 67 ppm, methyl glycolate at 60 ppm, and methyl formate at 51 ppm. Calibration ¹³C NMR spectra of mixtures of methyl lactate : methyl glycolate : xylose with given molar ratios of components of 0.5:1:1 were previously recorded. Xylose conversion (*X*) and product selectivity (*Y*, mol %) were calculated according to Eqs:

$$X (\text{mol}\%) = \frac{[\text{xylose}]_i - [\text{xylose}]_{pr}}{[\text{xylose}]_i} * 100,$$

$$S (\text{mol}\%) = *100.$$

RESULTS

The results of thermal analysis of the not-calcined samples are shown in Fig. 1. In the derivatograms of the CeO₂-SnO₂/Al₂O₃ and CuO-SnO₂/Al₂O₃ samples, only one endothermic effect was observed with mass loss in the region of 140–180 °C, caused by the condensation of

structural OH-groups with water release. The total weight loss of samples after heating to 1000 °C is 16.6 and 31.9 % by mass respectively. For the $\text{MoO}_3\text{-SnO}_2/\text{Al}_2\text{O}_3$ sample, two additional endo-effects appear with mass loss at 300 and ~ 375 °C, caused by the decomposition of the deposited

molybdenum (VI) salt [10]. The total weight loss of the sample after heating to 1000 °C is 39.7 % by mass. Thermogravimetric data showed the same good trend in thermal stability of all prepared samples.

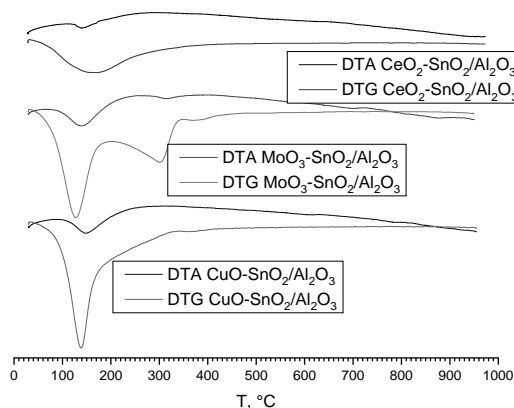


Fig. 1. The TGA/DTG curves of $\text{MeO-SnO}_2/\text{Al}_2\text{O}_3$ samples, dried at 120 °C (4 h) (heating rate - 10 °C/min)

As can be seen from the diffraction patterns (Fig. 2) of $\text{SnO}_2/\text{Al}_2\text{O}_3$ and $\text{MoO}_3\text{-SnO}_2/\text{Al}_2\text{O}_3$ samples, no crystalline Sn or Mo species could be detected, that indicates their well dispersed on the alumina surface forming small domains not detectable by XRD. It is interesting that the $\text{CuO-SnO}_2/\text{Al}_2\text{O}_3$ spectrum reveals the formation of the tetragonal rutile SnO_2 (JCPDS-41-1445) crystal structure and space group-P42/mnm, indicates by narrow peaks centered about 26.6°; 33.9°; 38.0° and 51.8 [11]. The introduction of copper oxide promotes the agglomeration of SnO_2 particles in the $\text{CuO-SnO}_2/\text{Al}_2\text{O}_3$ sample, while no peaks characteristic of CuO are observed. For the $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ sample intense diffraction

peaks at 28.66°; 33.08°; 47.47°; 56.36°; 59.08°; 69.40°; 76.70°; 79.07° and 88.41° are observed, which correspond to the cubic fluorite phase CeO_2 (JCPDS-34-0394) and space group-Fm3m [12]. Wherein there are no any characteristic peaks belong to SnO_2 . The main intensive diffraction peak located at $2\theta = 28.66^\circ$ corresponds to the (111) facet, that is the most thermodynamically stable [13]. It is known that the (111) facet is exposed when CeO_2 crystals have the shape of octahedra.

The formation of morphology ceria close to octahedra is confirmed by SEM microphotographs of the $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ sample (Fig. 3).

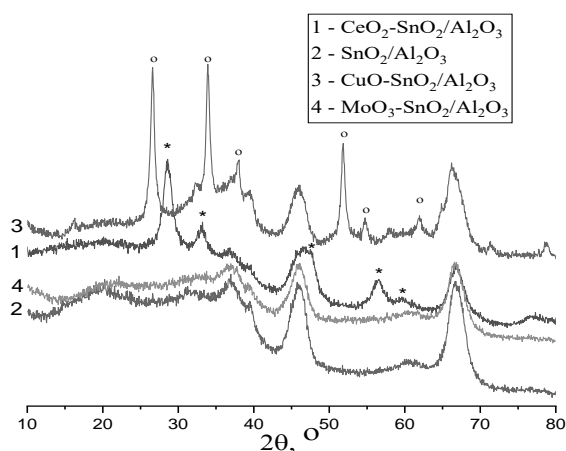


Fig. 2. XRD spectra of $\text{MeO-SnO}_2/\text{Al}_2\text{O}_3$ samples after calcination at 550 °C (* – CeO_2 , o – SnO_2)

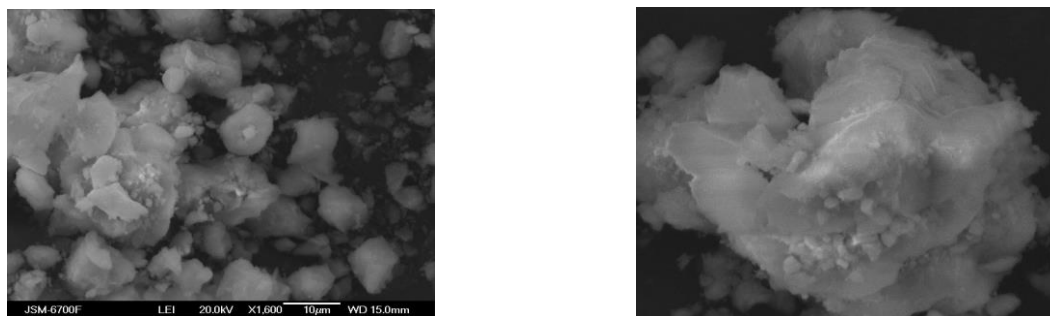


Fig. 3. SEM microphotographs of CeO₂-SnO₂/Al₂O₃ sample

Fig. 4 illustrates the band gap for the synthesized MeO-SnO₂/Al₂O₃ samples obtained from the electronic diffuse reflection spectra. For the SnO₂/Al₂O₃ sample the band gap is 4.5 eV, which indicates the nanosize of tin dioxide particles on the γ -Al₂O₃ surface [14]. Doping with metal oxides shifts the band gap to low energies. Thus, for the MoO₃-SnO₂/Al₂O₃ sample $E_g = 3.7$ eV, which indicates the presence of amorphous molybdenum oxide on its surface. Since, according to literature data [15], for

massive MoO₃, which is in an amorphous state, E_g is in the region of 2.7–3.2 eV, and the band gap of crystalline orthorhombic MoO₃ is about 1.95 eV. For the CuO-SnO₂/Al₂O₃ sample, $E_g = 3.7$ eV, which indicates the presence of massive SnO₂ phase on its surface [16]. The band gap for CeO₂ is known to be 2.9 eV [17], which is close to the band gap value of the CeO₂-SnO₂/Al₂O₃ sample ($E_g = 3.25$ eV). Thus, the UV spectroscopy data are consistent with the X-ray phase analysis data for all synthesized samples.

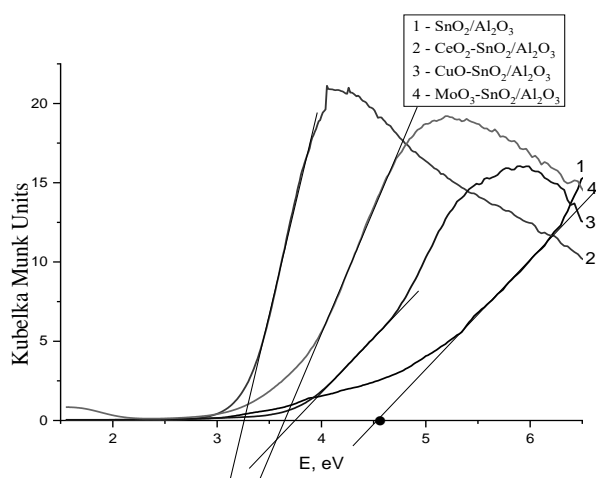


Fig. 4. Optical energy band gap of MeO-SnO₂/Al₂O₃ samples

Table 1. Textural and acidic characteristics of synthesized mixed oxides

Sample	Composition	Textural characteristics			Acidic characteristics	
		Specific surface area, m ² /g	Pore volume, cm ³ /g	Average pore radius, nm	Acid strength H_0	Total acidity, mmol/g
SnO ₂	-	39	0.07	3.6	+1.5	0.4
Al ₂ O ₃	-	290	0.86	5.3	+3.3	1.2
SnO ₂ /Al ₂ O ₃	10 % SnO ₂	250	0.67	5.7	+1.5	1.3
MoO ₃ -SnO ₂ /Al ₂ O ₃	10 % SnO ₂ , 5 % MoO ₃	230	0.63	5.6	+3.3	1.3
CuO-SnO ₂ /Al ₂ O ₃	10 % SnO ₂ , 5 % CuO	170	0.55	6.4	-	1.0
CeO ₂ -SnO ₂ /Al ₂ O ₃	10 % SnO ₂ , 5 % CeO ₂	200	0.61	6.2	-3.0	0.8

In Table 1 textural characteristics summarized are, as well as strength and concentration of acid sites of synthesized mixed oxides. All samples are mesoporous with a developed surface.

According to the titration results, $\text{SnO}_2/\text{Al}_2\text{O}_3$ is weakly acid mixed oxide with $H_0 \leq +1.5$ (Table 1). The addition of CeO_2 significantly increases the strength of acid sites of $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ samples to $H_0 \leq -3.0$. The acid-base properties of ceria are well known, namely the presence of surface O^{2-} ions as base L-sites and Ce^{4+} ions as acid L-sites, as well as hydroxyl groups as Brønsted basic sites [19]. Strength of Lewis acid sites as surface Ce^{4+} cations is barely dependent on the morphology of the ceria nanocrystals. It was found that octahedra have the smallest number and strength of the base sites [18, 19]. The article [19] presents IR and NMR data that indicate moderate Lewis acid strength of cerium cations on the surface of ceria-based catalysts.

The synthesized $\text{MeO-SnO}_2/\text{Al}_2\text{O}_3$ samples were further tested as catalysts for the reaction of

retro-aldol xylose condensation into methyl lactate (ML) in rotated autoclave (Table 2). According to the results of the products analysis, 100 % xylose conversion occurs only for $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst with a methyl lactate selectivity of 21 %. At the same time, a large amount of acetal and hemiacetal of pyruval are formed. In [20] it was noted that these acetals are the main products in the conversion of dihydroxyacetone-ethanol mixture over typical solid acids Amberlyst 15 and $\text{ZrO}_2\text{-SiO}_2$.

It should be noted that almost all tin dioxide was leached out from the surface of the $\text{CuO-SnO}_2/\text{Al}_2\text{O}_3$ catalyst during the reaction and $\text{MoO}_3\text{-SnO}_2/\text{Al}_2\text{O}_3$ oxide does not provide 100 % conversion of xylose (Table 2). Therefore, $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst was chosen for further studies in flow regime.

Results of xylose conversion carried out in a flow reactor at different temperature on $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst in air flow are presented in Table 3.

Table 2. Xylose conversion to methyl lactate over various catalysts¹

Catalyst	Conversion of xylose, %	Reaction products			
		ML	Acetals	Fur	Others
$\text{SnO}_2/\text{Al}_2\text{O}_3$	90	28	19	11	32
$\text{MoO}_3\text{-SnO}_2/\text{Al}_2\text{O}_3$	88	19	55	13	3
$\text{CuO-SnO}_2/\text{Al}_2\text{O}_3$	78	33	45	-	-
$\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$	100	21	79	-	-

¹ Reaction conditions: 1.1 g xylose, 0.68 g catalyst, 10 g 99 % methanol, 160 °C, 3 h; ML – methyl lactate, Fur– furans, Others – unidentified products

Table 3. Xylose conversion to reaction products at different temperatures on $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst¹

Temperature, °C	The composition of the reaction products, mol%				
	ML	MG	MF	Fur	Others
160	10	3	-	15	72
170	16	5	6	12	61
180	37	14	13	11	25
190	42	24	15	10	9

¹ Reaction conditions: 4 % xylose solution in a 70 % aqueous methanol solution, 3.0 MPa, $L = 3.5 \text{ mmol C}_5\text{H}_{10}\text{O}_5/\text{g}_{\text{cat}}/\text{h}$, air flow; ML – methyl lactate, MG– methyl glycolate, MF – methyl formate, Fur– furans, Others – unidentified products

Conversion of xylose is 100 % in the entire studied temperature range because the signals of D-xylopyranose in the range of 98–62 ppm were not observed in the ¹³C NMR spectra of reaction products (Fig. 5).

As shown in Table 3, with an increase in the reaction temperature, the selectivity of side methyl formate grows while yield of other by-products decreases. A further increase in, the reaction temperature up to 200 °C leads to

intensive formation of gaseous CO_2 . The temperature dependences of yield of targeted ML and MG are shown in Fig. 6.

Thus, at 190 °C, 3.0 MPa in air flow, a complete conversion of xylose occurs with the

formation of methyl lactate (42 %) and methyl glycolate (24 %) on the developed $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst at a loading of 3.5 mmol $\text{C}_5\text{H}_{10}\text{O}_5/\text{g}_{\text{cat}}/\text{h}$.

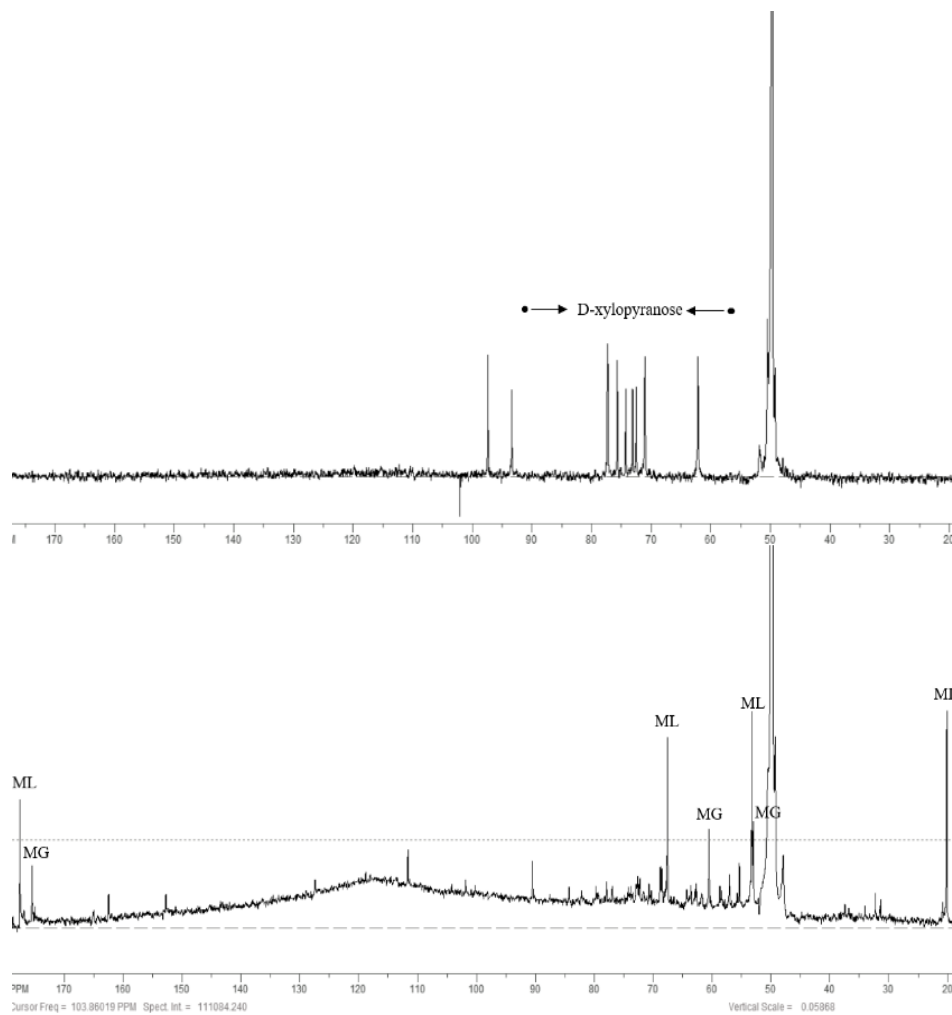


Fig. 5. ^{13}C NMR spectra of xylose (5 % xylose solution in a 70 % aqueous methanol solution) and reaction products

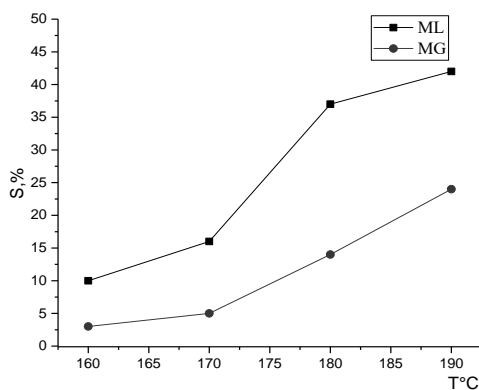
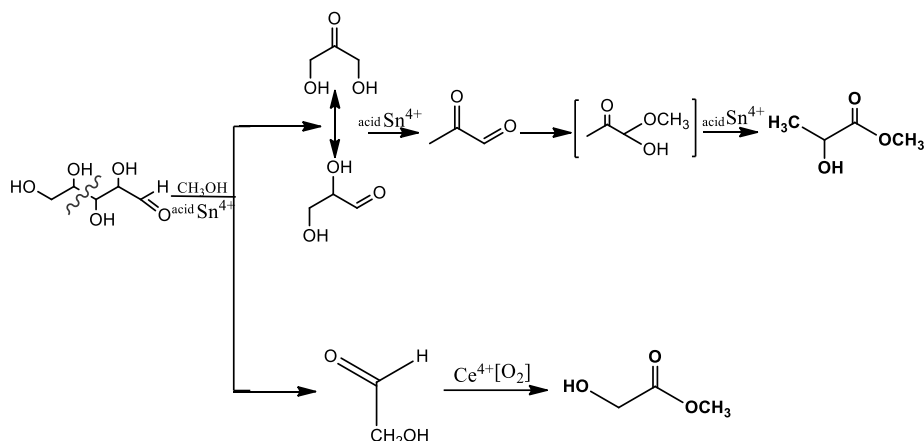


Fig. 6. Methyl lactate and methyl glycolate yields at different temperature on $\text{CeO}_2\text{-SnO}_2/\text{Al}_2\text{O}_3$ catalyst ($L = 3.5 \text{ mmol C}_5\text{H}_{10}\text{O}_5/\text{g}_{\text{cat}}/\text{h}$)

The $IVSn^{4+}$ ions in CeO_2-SnO_2/Al_2O_3 catalyst as Lewis acid sites promote retro-aldol xylose condensation and further Cannizzaro rearrangement of intermediate methyl pyruval hemiacetal into methyl lactate (Scheme 1). And CeO_2 provides selective oxidation of glycol aldehyde formed as a result of aldol

decondensation of xylose to methyl glycolate. This involves a two-stage oxidation Mars-Krevelen mechanism, according to which, glycol aldehyde reacts with the original catalyst - an oxidant, and then the catalyst is reoxidized by air oxygen.



CONCLUSION

Thus, an effective catalyst for the conversion of xylose into methyl esters of glycolic and lactic acids has been proposed. It was shown that as a result of first stage of aldol decondensation of xylose on the acid $IVSn^{4+}$ L-sites of catalyst, glyceraldehyde and glycol aldehyde are formed. The acid $IVSn^{4+}$ sites can be obtained by simply impregnating the surface of $\gamma-Al_2O_3$ with nanosized tin dioxide particles, which is confirmed by UV spectroscopy data. The same $IVSn^{4+}$ ions contribute to the last stage of retro-aldol condensation of xylose, namely Cannizzaro rearrangement of intermediate methyl pyruval hemiacetal into methyl lactate. Further doping of SnO_2/Al_2O_3 with oxides having redox properties makes it possible to obtain a catalyst for the

oxidation of formed glycol aldehyde to methyl glycolate in methanol solution. It has been found that among the studied oxides namely ceria provides selective oxidation of glycol aldehyde to methyl glycolate. The formation of cubic fluorite phase of CeO_2 with the morphology close to octahedra for CeO_2-SnO_2/Al_2O_3 sample was confirmed by XRD and SEM methods. It was found that 4 wt. % solution of xylose in 70 % methanol is a suitable reaction mixture for obtaining methyl esters of glycolic and lactic acids over proposed CeO_2-SnO_2/Al_2O_3 catalyst at $190\ ^\circ C/3.0\ MPa$ in air flow. This catalyst provides a complete conversion of xylose with the formation of methyl lactate (42 mol. %) and methyl glycolate (24 mol. %) at load on a catalyst of $3.5\ mmol\ C_5H_{10}O_5/g_{cat}/h$.

Окиснення суміші ксилоза-метанол в метиллактат та метилгліколат на CeO₂-SnO₂/Al₂O₃ каталізаторі

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В останні роки розробка каталітичних методів конверсії ксилози як відновлюваної сировини в хімічні речовини з доданою вартістю, такі як естери молочної та гліколевої кислот, є предметом інтенсивних досліджень. Так, метиллактат і метилгліколат використовуються як вихідний матеріал для виробництва лактиду і гліколіду – важливих мономерів для виробництва біорозкладних полімерів. Метою даної роботи був пошук простого ефективного каталізатора для перетворення ксилози в метилові естери молочної та гліколевої кислот. Для цього методом імпрегування синтезували оловомісний оксид алюмінію, допований оксидами CeO₂, MoO₃ та CuO. Текстульні та структурні параметри одержаних змішаних MeO-SnO₂/Al₂O₃ оксидів оцінено за результатами низькотемпературної адсорбції-десорбції азоту та рентгенофазового аналізу. Формування морфології оксиду церію, близької до октаедра, для зразка CeO₂-SnO₂/Al₂O₃ підтверджено даними рентгенофазового аналізу та мікрофотографіями SEM. Дані УФ-спектроскопії вказують на нанорозмір частинок діоксиду олова на поверхні γ-Al₂O₃. За результатами титрування CeO₂-SnO₂/Al₂O₃ є кислотним змішаним оксидом з H₀ ≤ -3.0. Каталітичну конверсію розчину ксилози в метанолі проводили в автоклавах, що обертаються, і в проточному реакторі з нержавіючої сталі з нерухомим шаром каталізатора. Продукти цільової реакції C₅H₁₀O₅+2CH₃OH+1/2O₂=C₄H₈O₃+C₃H₆O₃+2H₂O аналізували методом ¹³C ЯМР. Встановлено, що повна конверсія 4 % розчину ксилози в 70 % водному розчині метанолу відбувається з утворенням метиллактату (42 %) і метилгліколяту (24 %) на розробленому каталізаторі CeO₂-SnO₂/Al₂O₃ з навантаженням 3.5 ммоль C₅H₁₀O₅/г_{кат}/год при 190 °C/3.0 МПа в потоці повітря. Запропоновано шлях реакції, а саме: іони ^{IV}Sn⁴⁺ каталізатора CeO₂-SnO₂/Al₂O₃ як кислотні центри Льюїса сприяють ретро-альдольній конденсації ксилози та подальшому перегрупуванню Канніццаро проміжного напівацеталу пірвіноградного альдегіду в метиллактат. А CeO₂ забезпечує селективне окиснення гліколевого альдегіду, що утворюється в результаті альдольної деконденсації ксилози, до метилгліколяту.

Ключові слова: конверсія ксилози, метиллактат, метилгліколат, змішані оксиди, CeO₂, SnO₂

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Received 31.01.2024, accepted 03.09.2024